

## NANOREACTORS AND METHOD OF MAKING

### STATEMENT AS TO RIGHTS TO INVENTIONS MADE UNDER FEDERALLY SPONSORED RESEARCH OR DEVELOPMENT

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The invention described and claimed herein was made in part utilizing funds supplied by the United States Department of Energy under contract NO. DE-AC03-76SF000-98 between the United States Department of Energy and The Regents of the University of California. The government has certain rights to the invention.

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### PRIORITY

This application claims priority to U.S. Provisional application 60/555,590, filed March 22, 2004, and to International Application PCT/US04/33581, filed October 11, 2004, the contents of which are both incorporated herein by reference for all purposes.

### BACKGROUND OF THE INVENTION

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Porous solid materials are important in many areas of modern science and technology, including ion exchange, molecular separation, catalysis, chromatography, microelectronics, and energy storage. Notable examples are microporous (< 2 nm) zeolites and mesoporous (2-50 nm) silicate and carbonaceous materials. The ability to manipulate the structure and morphology of porous solids on a nanometer scale would enable greater control of chemical reactions.

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It is known that porosity may result from differential solid-state diffusion rates of the reactants in an alloying or oxidation reaction. Previous studies on the interdiffusion of 30-micrometer powders with layered composition showed significant porosity, but the

geometry and distribution of the pores were not uniform, probably due to aggregation and still bulk-like dimension of the particles. Recently, significant progress has been made in synthesizing colloidal nanocrystals with well-controlled size, shape and surface properties. This invention discloses the production of a uniform population of 5 nanoreactors by employing such high-quality nanocrystals as the starting materials.

Hollow particles of silica have been made with diameters between 720 and 1000 nm, see *Science*, Vol 282, Issue 5391, 1111-1114, 6 November 1998, the contents of which are hereby incorporated by reference in its entirety for all purposes.

Gold single crystalline nanoboxes have been made, though not on the nanoscale 10 size dimension as taught by the present invention, see Y. Sun, Y. Xia, *Science* 298, 2176 (2002), the contents of which are hereby incorporated herein in its entirety for all purposes.

#### SUMMARY OF THE INVENTION

This invention discloses the production of a uniform population of nanoreactors. 15 The nanoreactors comprise a nanoreactor shell having a thickness of at least 0.5 nm, And the nanoreactor shell envelops or encages a space. The nanoreactor shell is not perfectly single crystalline and a nanoparticle disposed within the space.

Also disclosed is a method of making a nanoreactor, comprising providing a nanoparticle, coating the nanoparticle with a first material, 20 reacting the first material with a second material, wherein the first and second material react to form a nanoreactor shell encaging the nanoparticle.

### BRIEF DESCRIPTION OF THE DRAWINGS

**FIG 1A** Pt nanoparticles prepared in accordance with this invention.

**FIG 1B** Pt@CoO nanoreactors formed in accordance with one embodiment of the present invention.

### 5 DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

By "providing a nanocrystal or nanoparticle" it is meant any step, process or manipulation that produces a nanocrystal or nanoparticle capable of entering into a reaction or process. Typically this step is synthetic, and the nanocrystals or particles are in solution after synthesis. This step may be accomplished by purchasing commercially available nanocrystals or nanoparticles.

10 By "bulk" or "bulk systems" it is meant materials not on the nanoscale size dimension.

By "disk shaped" or "disk" it is meant a relatively cylindrical structure having size dimensions as defined herein.

15 By "tube shaped" or "tubular" and "tube(s)" it is meant a structure that has a hollow cylindrical shape. The cylinder is not required to be uniform in diameter. It is understood that the tube has two ends that are closed. However, during synthesis it is possible for the ends to become open by accidental fracture.

20 By "nanoreactor" it is meant to include all shapes, including spheres, disks, tubes, tetrapods, branched and unbranched nanocrystals. As used herein, a particle enclosed in a nanocrystal shell is termed a "nanoreactor" a "nanocatalyst" a "nanosphere", "yolk/shell" and also "Pt@CoO" or Pt/CoO (note: Pt and CoO are only non-limited examples of materials).

By "preliminary main material" as recited herein it is meant the first material, also termed the main starting material, not the nanoparticle such as Pt, in the present invention, which is an element, a compound or a composition that is coated over the nanoparticle. This material reacts to form a nanocrystal shell with a space around the nanoparticle enclosed therein.

5 By "reaction" it is meant to include not only chemical reactions, but also alloy formation.

By "not perfectly single crystalline" it is meant that there are at least grain boundaries or other defects in the nanoreactor shell.

10 By "envelop" it is meant to enclose completely with or as if with a covering. This definition allows for the presence of grain boundaries due to polycrystalline materials.

15 By "Pt@CoO" or "Pt/CoO" it is meant Pt particles in a CoO shell, where there is space between the inside particle and the inside wall of the shell. It is understood that the CoO shell is only one non-limiting example of the material contemplated for the shell, as well as Pt particles as non limiting examples for the nanoparticle enclosed within the shell. The term "yolk/shell" refers to a CoO shell and a Pt yolk in this instance.

The nanoreactors produced in accordance with the present invention have outside diameters of between about 1 nm-1000 nm. In a preferred embodiment the nanoreactor have outside diameters of between 1 nm-500 nm and more preferred is about 5 nm-100 nm, even more preferred are 10 nm-50 nm, and even more preferred are 10 nm-30 nm. In one embodiment nanotubes have outside diameters of between about 1 nm-1000 nm, preferably between 5 nm - 500 nm, and more preferably between about 10 nm-250 nm, and even more preferably between 10 nm-100 nm. The length of the nanotubes used

as nanoreactors herein in accordance with the present invention ranges from about 30 nm to 500  $\mu$ m, preferably between about 30 nm -250  $\mu$ m and more preferably between about 50 nm and 200  $\mu$ m, even more preferably between 50 nm-20  $\mu$ m. In one embodiment nanoreactors with a disk shape have diameters between 10 nm -200 nm, preferably 5 between about 10 nm -100 nm and more preferably about 25 nm-50 nm. In one embodiment the thickness of the disk is between about 1 nm-20 nm, preferably between 2 nm-15 nm and more preferably between 3 nm-10 nm.

The ratio of the inside diameter (id) to the outside diameter (od) for nanoreactors, expressed (id)/(od), ranges from between 20-90%. As a non-limiting example CoO and 10 CoS nanospheres made in accordance with this invention have a ratio of about 40%.

The present invention contemplates that the thickness of the nanoreactor wall is controllable by varying the temperature of the reaction and the concentration of the material that reacts with the preliminary main material to form the nanocrystal shell of the nanoreactor. In one embodiment of the invention the walls or shell of the 15 nanoreactor have a thickness having a range between 0.5 nm and 100 nm, preferably between 2 nm-80 nm and more preferably between 3 nm-50 nm, even more preferably between about 3 nm and 10 nm. By varying the reaction temperature and concentration, the (id)/(od) for CoS may vary between 30%-40% (.3-.4). In a preferred embodiment of the method, it is preferable to control the (id)/(od) by varying the preliminary starting 20 nanoreactor size.

It is understood that in accordance with this invention the shell of the nanoreactors from a continuous three dimensional domain adopting a three dimensional arrangement of atoms in contrast to molecular sheets such as found in graphitic, WS<sub>2</sub> or

MoS<sub>2</sub> nanotubes and nanocages.

The crystallinity of the nanoreactor wall, or shell is controllable. In a preferred embodiment the shell is at least partially crystalline. The advantage of a polycrystalline shell is that the defective grain boundary will allow gasses and other chemical species made of small molecules to permeate. One skilled in the art will appreciate that annealing at relatively high temperatures will eliminate many grain boundaries. In one embodiment of the present invention the nanoreactors have an extremely low crystallinity, so as to be almost amorphous. The nanoreactors in the present invention have shell walls that are nanocrystals that are not perfectly single crystalline. In a preferred embodiment the nanoreactors are at least partially polycrystalline. In a more preferred embodiment they are between 10-100 % polycrystalline, and in a more preferred embodiment they are between 50 and 100% polycrystalline, and in an even more preferred embodiment they are between 75 and 100% polycrystalline. The percentages as used herein refer to the total volume fraction of the crystalline grains in the nanoreactor excepting the largest crystalline grain.

In one embodiment of the present invention a nanoreactor is provided which may be used as a catalytic material. In one non-limiting embodiment a Pt@CoO nanoreactor is synthesized, in which a Pt nanoparticle of a few nanometers is encapsulated in a CoO shell. Generally, three steps are involved in the preparation of these nanoreactors: synthesis of nanoparticle seeds, in this embodiment Pt seeds are provided by a modified "polyol" process, as in N. S. Sobal, U. Ebels, H. Möhwald, M. Giersig, *J. Phys. Chem.* 107, 7351 (2003) the contents of which are hereby incorporated by reference in its entirety. The present invention contemplates that any metal, material or alloy capable of

catalytic activity is useful. The size of the particles can be tuned from at least .5 to 20 nm, preferably 1-10 nm, more preferably 2-5 nm, typically depending on the concentration and choice of surfactants. Any shape particle may be used. Any particle made using other methods may also be used.

5       The second step involves deposition of a first material termed the preliminary main material herein, in one non limiting embodiment cobalt, on the nanoparticle, in this embodiment, Pt. In one embodiment this is accomplished by injecting  $\text{Co}_2(\text{CO})_8$  into a hot solution of nanoparticles and decomposed to form a conformal coating on Pt nanoparticles. Tertiarily is the transformation of the preliminary main material, in this case, Co into CoO hollow structures. In one embodiment of the present invention this is accomplished by the following oxidation procedure. Oxidation of the Pt@Co nanocrystals is performed a few minutes after the introduction of cobalt carbonyl by blowing a stream of  $\text{O}_2/\text{Ar}$  (1:4 in volume ratio, 120 ml/min) mixture into the colloidal solution at 455 K. The system is kept under stirring for 3 hours. A black stable colloidal dispersion in *o*-dichlorobenzene is obtained. Finally, the Pt@CoO nanoreactors are precipitated by methanol, washed with toluene and methanol three times, and dried under vacuum. Typical nitrogen adsorption/desorption measurement on the powder at 77K shows a type IV isotherm with type H2 hysteresis, with a Brunauer-Emmet-Teller (BET) surface area of  $65 \text{ m}^2/\text{g}$  and a total pore volume of  $0.0676 \text{ cm}^3/\text{g}$ . FIG 1A shows a typical sample of Pt particles with an average diameter around 3 nm. The deposition of Co onto Pt at the reaction temperature yields no alloy, only Pt core/Co shell particles, as confirmed by XRD analyses. The oxidation reaction removes Co atoms away from the Pt particle surface, leading to the formation of a Pt yolk/CoO shell structure (FIG 1B). No

free platinum particles were found by TEM inspections on the Pt@CoO sample.

In one embodiment of the present invention, sulfidation of a preliminary main starting material such as cobalt results in formation of the nanoreactor shell. Cobalt sulfide shells are synthesized in one pot by injection of a solution of sulfur in *o*-dichlorobenzene into a hot Co capped nanoparticle. At 445 K, the reaction between cobalt and sulfur completes within a few seconds, resulting in a stable black solution of cobalt sulfide hollow nanocrystals with a nanoparticle enclosed therein.

During the reaction of the sulfur with the hot nanocrystal solution, outward flow of cobalt through the sulfide shell results in supersaturation of vacancies, which condense to form a single hole in each nanoparticle. Two stable cobalt sulfide phases are observed, linnaeite ( $\text{Co}_3\text{S}_4$ ) and cobalt pentlandite ( $\text{Co}_9\text{S}_8$ ), depending on the sulfur-to-cobalt molar ratio used in the synthesis. One having ordinary skill in the art will be able to adjust the sulfur-to-cobalt ration to arrive at the desired composition of linnaeite and pentlandite.

In one embodiment of the present invention, the outside starting nanocrystal shell material may be reacted with oxygen to produce oxide shell nanocrystals. In one nonlimiting embodiment, bulk cobalt, the rates of oxidation are 3-4 orders of magnitude lower than those of sulfidation above 750 K, see S. Mrowec, M. Danlelewski, A. Wojtowicz, *J. Mater. Sci.* 33, 2617 (1998), the contents of which are hereby incorporated by reference for all purposes.

In another embodiment of the present invention, the outside starting nanocrystal shell material may be reacted with selenium to produce shell nanocrystals, for example cobalt may be reacted with selenium. In bulk systems, annihilation of excess

vacancies at dislocations and boundaries can produce stresses leading to the formation of cracks near the interface; the cracks then act as nuclei for the further condensation of supersaturated vacancies, see F. Aldinger, *Acta Met.* **22**, 923 (1974), the contents of which are hereby incorporated by reference in its entirety for all purposes. While the  
5 exact mechanism is likely to be different, in nanocrystals voids also begin to develop and merge at the boundary. The high defect content and surface energy associated with the boundary favors the nucleation of voids there. Also, as vacancies diffuse inwards, they will be more concentrated at the boundary rather than in the interior of the core. As the reaction proceeds in time, more cobalt atoms diffuse out to the shell and the  
10 accompanying transport of vacancies leads to growth and merging of the initial voids. This results in the formation of bridges of material between the core and the shell that persist until the core is completely consumed. These bridges provide a fast transport path for outward diffusion of cobalt atoms which can then spread on the inner shell surface. A similar phenomenon was observed for bulk powders.

15 Disk shaped nanoreactors may be made in accordance with one embodiment of this invention, where the nanoparticle has a disk shape. The starting material or first nanocrystal must have a disk shape. Disk shaped particles may be made according to the prior art methods such as V. F. Puntes, D. Zanchet, C. K. Erdonmez, A. P. Alivisatos, *J. Am. Chem. Soc.* **124**, 12874 (2002), the contents of which are hereby incorporated by  
20 reference in its entirety for all purposes.

The material used as a nanoparticle for the nanoreactor may be elemental or a compound, or an alloy. In a preferred embodiment the material used as a nanoparticle be elemental. Metals include the main group metals, Al, Ga, In, Tl, Sn, Pb, Bi and Po; the

transition metals Sc, Ti, V, Cr, Mn, Fe, Co, Ni, Cu, Y, Zr, Nb, Mo, Tc, Ru, Rh, Pd, Ag, Cd, La, Hf, Ta, W, Re, Os, Ir, Pt, Au, Hg, the alkali and alkaline earth metals Li, Na, K, Rb, Cs, Be, Mg, Ca, Sr, Ba and the semiconductor metals Ge, Si, Se, Te. Compounds include, but are not limited to  $\text{Fe}_2\text{O}_3$ ,  $\text{TiO}_2$ , CdS, CdSe and ZnS. Alloys include, but are 5 not limited to FeCo, CoNi and CdZn. Preferred in Pt metal.

The material used as a preliminary main material for the outside shell of the nanoreactor may be elemental or an alloy. In a preferred embodiment the preliminary main material for the formation of nanoreactors be elemental. Metals include the main group metals, Al, Ga, In, Tl, Sn, Pb, Bi and Po; the transition metals Sc, Ti, V, Cr, Mn, 10 Fe, Co, Ni, Cu, Y, Zr, Nb, Mo, Tc, Ru, Rh, Pd, Ag, Cd, La, Hf, Ta, W, Re, Os, Ir, Pt, Au, Hg, the alkali and alkaline earth metals Li, Na, K, Rb, Cs, Be, Mg, Ca, Sr, Ba and the semiconductor metals Ge, Si, Se, Te. Alloys include, but are not limited to FeCo, CoNi and CdZn. It would not be possible to obtain structures containing carbon as the major constituent material, but various carbon nanostructures, including diamond nanoparticles 15 or carbon nanotubes may be utilized as the starting material and reacted with other species to obtain carbon-alloyed nanoreactors, for example nanospheres of steel may be synthesized by reacting a diamond nanospheres with a suitable iron source. This resulting structure will be chemically and crystallographically very different from sheet-like structures such as buckminsterfullerenes or carbon nanotubes. Halogens and noble 20 gases are not suitable. One having ordinary skill in the art will appreciate that the stability and reactivity of the preliminary main material in solution and under reaction conditions will impact on the success of the present method and the quality of the nanoshell derived therefrom. For example, alkali earth metals are less stable and would

require more stringent reaction conditions for success.

The material chosen to react with the material used as a preliminary main material does not have to be elemental. It is only required that the material be capable of donating that element or compound of interest. As a non-limiting example, for the sulfidation of 5 Co, all that is required is a compound capable of donating sulfur. One skilled in the art will readily appreciate without undue experimentation the compositions capable of donating sulfur in the reaction solution.

As non-limiting examples, nanoreactors in accordance with the present invention have shells that may comprise ZnS, ZnSe, ZnTe, ZnO and other oxides of the preliminary 10 main materials such as CoO, Co<sub>3</sub>O<sub>4</sub>, Fe<sub>2</sub>O<sub>3</sub>, TiO<sub>2</sub> and Al<sub>2</sub>O<sub>3</sub>; Cd materials coated over a nanoparticle such as Pt may produce cadmium nanoshells such as CdS by sulfidation; other non-limiting examples of sulfur compounds include those of other metals including 15 Ni, such as Ni<sub>5</sub>S<sub>2</sub>; other Ni compounds include Ni<sub>2</sub>Si, NiSi and NiCl<sub>2</sub>; other cadmium compounds include CdSe, CdTe, etc.; though difficult, Hg materials may produce HgS, HgSe, HgTe; other nanocrystals include MgTe and the like, GaN, GaP, GaAs, GaSb, InN, InP, InAs, InSb, AlAs, AlP, AlSb, AlS, and the like, Co<sub>9</sub>S<sub>8</sub>, Co<sub>3</sub>S<sub>4</sub> and CoSe. Also included are ternary material systems such as GaMnAs, GaInN and InAsN.

In accordance with the present invention, the mobilities of the reacting species, the first material i.e. the preliminary main material and the second material are 20 not necessarily chosen such that they are drastically different to result in vacancy transport. The invention contemplates that placing a nanoparticle having a coating comprising one reactant in a comparatively dilute solution creates an additional asymmetry that may favor the creation of nanospheres encaging a nanoparticle.

The present invention contemplates that the nanoreactors of the present invention may serve as heterogeneous catalysts. This invention contemplates platinum or other suitable inside nanoparticle can carry out hydrocarbon conversion reactions (which includes any reaction that includes a hydrocarbon as feedstock without any participation of the cobalt oxide shell. These reactions include hydrogenation, dehydrogenation of ethylene and cyclohexene. A preferred embodiment is the use of the nanoreactors disclosed in for the isomerization of hydrocarbons. By "hydrocarbons" it is meant to include C<sub>4</sub>-C<sub>3000</sub>, preferred is C<sub>4</sub>-C<sub>10</sub>. One advantage of the present nanoreactors over the prior art is that the separation of the nanoparticles by the nanocrystal shell prevents secondary reaction of the products that would change selectivity and desired product distribution. In other embodiment it is contemplated that at higher reaction temperatures, both the cobalt compound and the Pt nanoparticle inside the shell are active. In this circumstance, the reaction selectivity can be altered because Pt readily atomizes H<sub>2</sub> or O<sub>2</sub> to provide superior reducing or oxidizing power for the cobalt compound. Reactions of interest include CO hydrogenation, partial oxidation of light alkanes and hydrodesulfurization of thiophene. In a preferred embodiment the hydrodesulfurization of thiophene is carried out by contacting thiophene with the nanoreactors described herein during a hydrodesulfurization process. Hydrodesulfurization is known in the art and is heretofor catalyzed by other materials.

To demonstrate the efficiency of the nanoreactors described herein, Pt@CoO was chosen to exemplify a heterogeneous catalyst and the hydrogenation of ethylene was chosen as a model reaction since it readily occurs at ambient conditions on many transition metal catalysts. Platinum is one of the most active metals for this reaction

while the activity of metallic cobalt is approximately two orders of magnitude lower. Pure CoO hollow nanocrystals are inactive for ethylene hydrogenation even following a 1 h H<sub>2</sub> pre-reduction at 373 K. Only upon reduction at 473 K for 1 h is ethane detected at temperatures >300 K. However, in accordance with one embodiment of the present invention samples containing Pt are active for C<sub>2</sub>H<sub>4</sub> hydrogenation at temperatures as low as 208 K, with samples subjected to no pretreatment. The steady state turnover frequency for ethane formation at 227 K is  $8.3 \times 10^{-3} \text{ s}^{-1}$ , which is comparable to rate of  $3.5 \times 10^{-2} \text{ s}^{-1}$  measured on a 0.04% Pt/SiO<sub>2</sub> catalyst. Comparison of reaction rates (on per gram total catalyst basis) at 300 K demonstrate that Pt@CoO is 2 orders of magnitude more active than CoO. These observations indicate that the reaction is catalyzed by Pt particles, not the CoO shell. This also confirms that a route exists for ethylene and hydrogen entry into the CoO shell interior. While not wishing to be bound by any particular theory or principle, the grain boundaries on the shell are the most probable entry points for ethylene and hydrogen diffusion into as well as ethane diffusion out of the shell.

For the hydrogenation of ethylene (C<sub>2</sub>H<sub>4</sub>) catalyzed by Pt/CoO nanocatalysts, the measurements were carried out in a gas handling manifold/atmospheric plug flow reactor (PFR) constructed of 1/4" O.D. pyrex tubing. Gas flowrates were controlled with mass flow controllers (MKS Instruments) and all gases (He, H<sub>2</sub> and C<sub>2</sub>H<sub>4</sub>) were released into a central 1/8" O.D. stainless steel manifold connected to the pyrex manifold. The plug flow reactor was a U-tube of 1/4" O.D. pyrex tubing with a porous pyrex frit for catalyst support. A thermocouple sheath made of 1/8" I.D. pyrex was inserted into the reactor for catalyst bed temperature measurements during reaction using a thermocouple (Omega Engineering Inc., Type K, 1/8" diameter). All ethylene hydrogenation reactions were

conducted at sub-ambient conditions using organic solvent/liquid nitrogen slush baths, see Rondeau, R. E. *J. Chem. Eng. Data* **11**, 124 (1966), the contents of which are hereby incorporated by reference in its entirety for all purposes. After stabilization of the slush bath temperature, the reactor was submersed in the bath. Reaction products were detected with a gas chromatograph (Hewlett Packard 5890 Series II) equipped with a flame ionization detector (FID). Reactants and products were separated with a homemade  $\text{Al}_2\text{O}_3$  column ( $\frac{1}{8}$ " O.D. stainless steel tubing, 10 foot coiled length). Ethylene and ethane concentrations are determined from the area counts from the GC after Dietz correction, see Dietz, W. A. *J. Gas Chrom.* **5**, 68 (1967). Typical reaction conditions were 10 Torr  $\text{C}_2\text{H}_4$ , 150 Torr  $\text{H}_2$  with balance He at a total flowrate of 90  $\text{cm}^3(\text{STP}) \text{ min}^{-1}$ . A gas chromatograph from the hydrogenation of ethylene over a 14.2% Pt(5.4 nm)/CoO material at room temperature shows the peak with a retention time of 2.9 minutes is ethane, while the larger peak at 4.0 minutes is ethylene. In a typical experiment, approximately 25-100 mg of sample was loaded into the reactor and purged with 50  $\text{cm}^3(\text{STP}) \text{ min}^{-1}$  He for 1 h followed by a 20%  $\text{H}_2/\text{He}$  mixture (88.5  $\text{cm}^3(\text{STP}) \text{ min}^{-1}$  total) for  $\frac{1}{2}$  h, after which the ethylene flow ( $1.5 \text{ cm}^3(\text{STP}) \text{ min}^{-1}$ ) was started. Pt containing CoO nanocrystals (nanoreactors) were characterized using physical adsorption measurements of nitrogen ( $\text{N}_2$ ) at -195°C (77 K). Total surface area, pore volume and pore size distribution were determined using an automated sorption analyzer (Quantachrome 1C). The total surface area was determined using the BET method, see S. Brunauer, P. Emmett, E. Teller, *J. Am. Chem. Soc.* **60**, 309 (1938), the contents of which are hereby incorporated by reference in its entirety. The total pore volume was determined with the Kelvin equation using the  $\text{N}_2$  uptake (at STP) at a

relative pressure ( $P/P_0$ ) of 0.975. Pore size distributions were determined by the Barrett-Joyner-Halenda (BJH) method, see E. P. Barrett, L. G. Joyner, P. P. Halenda, *J. Am. Chem. Soc.* **73**, 373 (1951), the contents of which are hereby incorporated by reference in its entirety for all purposes.

5 Average Pt particle sizes were determined from counting particles in representative TEM micrographs (FIG 1A). The method used has been described by Matyi *et al.*, see Matyi, R. J.; Schwartz, L. H.; Butt, J. B. *Catal. Rev. Sci Eng.* **29**, 41 (1987), the contents of which are hereby incorporated by reference in its entirety. TEM measurements of particle size represent a bulk measurement of particle size. The number 10 of surface atoms, which is related to the bulk particle size was determined from the expression,  $D = 1.13/d$ , where  $D$  is the dispersion (ratio of surface Pt atoms to the total number of Pt atoms) and  $d$  is the diameter of the nanoparticle in nm, see Yin, Y.; Rioux, R. M.; Erdonmez, C. K.; Hughes, S.; Somorjai, G. A.; Alivisatos, A. P. *Science* **304**, 711 (2004), the contents of which are hereby incorporated by reference in its entirety.

15 Determination of the number of surface Pt atoms enables catalytic rates (measured on a per gram total catalyst basis) to be normalized per mole of surface platinum, i.e. turnover frequency.

The adsorption/desorption isotherms of Pt/CoO nanoreactors were of type IV with type H<sub>2</sub> hysteresis. The BET surface area of the Pt/CoO nanorectors varied from 30-100 m<sup>2</sup> g<sup>-1</sup>. For example, a 14.2% Pt(5.4 nm)/CoO had a total surface area of 65 m<sup>2</sup> g<sup>-1</sup>. The 20 pore volume for the same 14.2% Pt/CoO catalyst was  $6.8 \times 10^{-2}$  cm<sup>3</sup>(STP) g<sup>-1</sup> at a  $P/P_0 = 0.975$ , while the BJH pore size was 3.6 nm.

### Examples

**Example 1: Synthesis of Pt@Co<sub>9</sub>S<sub>8</sub> nanoreactors**

Pt was provided by preparing platinum nanoparticles by injecting a solution of 0.15 g of platinum acetylacetone in 5 ml of *o*-dichlorobenzene into a refluxing bath of 10 ml of *o*-dichlorobenzene containing 0.3 g of 1,2-hexadecanediol, 0.1 ml of oleic acid, 0.1 ml of oleylamine and 0.06 ml of trioctylphosphine. The solution was then heated for another 5 120 minutes to yield Pt nanoparticles in solution. Pt@Co<sub>9</sub>S<sub>8</sub> nanoreactors are formed by injecting 1.08 g Co<sub>2</sub>(CO)<sub>8</sub> in 6 ml *o*-dichlorobenzene into the platinum nanocrystal solution followed by the sulfidation of the product particles by injecting a solution of 10 0.171 g sulfur in 10 ml of *o*-dichlorobenzene. The system was kept at the same temperature under stirring for 3 minutes. A black stable colloidal dispersion in *o*- dichlorobenzene is obtained. Finally, the Pt@Co<sub>9</sub>S<sub>8</sub> nanoreactors are precipitated by methanol, washed with toluene and methanol three times, and dried under vacuum. Nitrogen adsorption/desorption measurement on the powder at 77K shows a type IV isotherm with type H<sub>2</sub> hysteresis, with a Brunauer-Emmet-Teller (BET) surface area of 15 90 m<sup>2</sup>/g.

**Example 2****Synthesis of Pt@Co<sub>3</sub>S<sub>4</sub> nanoreactors**

Platinum nanoparticles are prepared by injecting a solution of 0.15 g of platinum acetylacetone in 5 ml of *o*-dichlorobenzene into a refluxing bath of 10 ml of *o*- dichlorobenzene containing 0.3 g of 1,2-hexadecanediol, 0.1 ml of oleic acid, 0.1 ml of 20 oleylamine and 0.06 ml of trioctylphosphine. The solution was then heated for another 120 minutes. Pt@Co<sub>3</sub>S<sub>4</sub> nanostructures are formed by injecting 1.08 g Co<sub>2</sub>(CO)<sub>8</sub> in 6 ml *o*-dichlorobenzene into the platinum nanoparticle solution followed by the sulfidation of

the product particles by injecting a solution of 0.256 g sulfur in 10 ml of *o*-dichlorobenzene. The system was kept at the same temperature under stirring for 3 minutes. A black stable colloidal dispersion in *o*-dichlorobenzene is obtained. Finally, the Pt@Co<sub>3</sub>S<sub>4</sub> particles are precipitated by methanol, washed with toluene and methanol three times, and dried under vacuum. Nitrogen adsorption/desorption measurement on the powder at 77K shows a type IV isotherm with type H2 hysteresis, with a Brunauer-Emmet-Teller (BET) surface area of 90 m<sup>2</sup>/g.

5 Example 3

Synthesis of Pt@CoO nanoreactors

10 Platinum nanoparticles are prepared by injecting a solution of 0.15 g of platinum acetylacetone in 5 ml of *o*-dichlorobenzene into a refluxing bath of 10 ml of *o*-dichlorobenzene containing 0.3 g of 1,2-hexadecanediol, 0.1 ml of oleic acid, 0.1 ml of oleylamine and 0.06 ml of trioctylphosphine. The solution was then heated for another 120 minutes. Pt@CoO nanostructures formed by injecting 1.08 g Co<sub>2</sub>(CO)<sub>8</sub> in 6 ml *o*-dichlorobenzene into the platinum nanocrystals solution, and followed by the oxidation of 15 the product particles by blowing a stream of O<sub>2</sub>/Ar (1:4 in volume ratio, 120 ml/min) mixture into the colloidal solution at 455 K. The system was kept at the same temperature under stirring for 3 hours. A black stable colloidal dispersion in *o*-dichlorobenzene is obtained. Finally, the Pt@CoO nanoreactors are precipitated by methanol, washed with toluene and methanol three times, and dried under vacuum. Typical nitrogen adsorption/desorption measurement on the powder at 77K shows a type 20 IV isotherm with type H2 hysteresis, with a Brunauer-Emmet-Teller (BET) surface area of 65 m<sup>2</sup>/g.

**Example 4: Catalytic activity of nanocatalysts**

The reactivity of 14.2% Pt(5.4 nm)/CoO nanoparticles for ethylene hydrogenation

A 14.2% Pt(5.4 nm)@CoO nanocatalyst was studied for catalytic ethylene hydrogenation

reactivity. Approximately 25 mg of Pt/CoO nanocatalyst was loaded in a plug flow

5 reactor and purged with 50 cm<sup>3</sup>(STP) min<sup>-1</sup> He for 1 h followed by a 20% H<sub>2</sub>/He mixture

(88.5 cm<sup>3</sup>(STP) min<sup>-1</sup> total) for ½ h, after which ethylene flow (1.5 cm<sup>3</sup>(STP) min<sup>-1</sup>) was

started. Upon contact of the ethylene and H<sub>2</sub> with the catalyst bed, a sharp exotherm was

measured by the thermocouple strategically placed in the catalyst bed. The

corresponding ethylene conversion was 100 %. This material maintained 100% ethylene

10 conversion at room temperature for more than 24 hours. In order to measure reaction

rates at conditions free of heat and mass transfer, the conversion and corresponding

temperature increase due to reaction were decreased by submersion of the reactor in a

sub-ambient temperature organic solvent-liquid nitrogen slush bath. Slush bath

temperatures were varied from 208-260 K and maintained ± 1 K by the frequent addition

15 of liquid nitrogen. At these temperatures, conversions varied from 1.5 – 14 %

conversion. Reaction rates at 227 K were reported as specific activity (μmol g<sub>cat</sub><sup>-1</sup> s<sup>-1</sup>)

and turnover frequencies (s<sup>-1</sup>). Turnover frequencies were normalized to the number of

surface Pt atoms assuming a particle size determined from TEM measurements and all Pt

was accessible to ethylene and hydrogen. The most active Pt/CoO nanoreactor had an

20 activity of 1.3 μmol g<sub>cat</sub><sup>-1</sup> s<sup>-1</sup> and a turnover frequency of 8.3 × 10<sup>-3</sup> s<sup>-1</sup> at 10 Torr C<sub>2</sub>H<sub>4</sub>,

150 Torr H<sub>2</sub> and 227 K. The ability of these Pt nanocatalysts confirms that ethylene and

hydrogen are able to penetrate the CoO shell structure and react on the surface of Pt.

While not wishing to be bound by any particular theory or principle, the most likely

points of entry for ethylene and H<sub>2</sub> into the interior are the grain boundaries present on the polycrystalline CoO shell.

**Example 5:** Reactivity of 4.2% Pt(3.8 nm)/CoO nanocatalysts for ethylene hydrogenation

5 Similar to example 4, a nanoreactor material with slightly smaller Pt particles (*ave.* 3.8 nm) was tested for ethylene hydrogenation in a plug flow reactor. Approximately 25 mg of catalyst was loaded in a plug flow reactor and purged with 50 cm<sup>3</sup>(STP) min<sup>-1</sup> He for 1 h followed by a 20% H<sub>2</sub>/He mixture (88.5 cm<sup>3</sup>(STP) min<sup>-1</sup> total) for ½ h, after which ethylene flow (1.5 cm<sup>3</sup>(STP) min<sup>-1</sup>) was started. Reaction rates were measured at sub ambient temperatures by means of liquid nitrogen slush baths. Temperatures were varied  
10 from 208-250 K. At these temperatures, conversions varied from 1 – 10 %. The 14.2% Pt(3.8 nm)/CoO nanoreactor catalyst had a turnover frequency of  $2 \times 10^{-3}$  s<sup>-1</sup> at 10 Torr C<sub>2</sub>H<sub>4</sub>, 150 Torr H<sub>2</sub> and 227 K.

Example 6: Synthesis of Pt@CoO nanoreactors with Pt nanoparticles of well-defined shapes. The invention contemplates that any shaped particle is suitable for the nanoparticle disposed in the nanoreactor. Dual sectioned nanoparticles are also contemplated as well as particles comprising two or more elements, in sections or alloys. The addition of sacrificial metal ions leads to the anisotropic growth of host metals in solution. Pt nanoparticles of ~ 7nm with well-defined shape have been synthesized by the addition of varying amounts of Ag ions to an ethylene glycol solution containing chloroplatinic acid (H<sub>2</sub>PtCl<sub>6</sub> · xH<sub>2</sub>O) and poly(vinylpyrrolidone) (PVP), see Song, H.; Kim, F.; Connor, S.; Somorjai, G. A.; Yang, P. *J. Phys. Chem. B* **109**, 188 (2005), the contents of which are hereby incorporated by reference in its entirety for all purposes.  
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Incorporation of Pt nanoparticles of well-defined shape into Co<sub>9</sub>S<sub>8</sub>, Co<sub>3</sub>S<sub>4</sub>, or CoO nanoreactors follows examples 1-3. Modification of the shape controlled Pt nanoparticle synthesis from Song *et al.* is required for Pt@CoO yolk-shell formation. Pt nanoparticles synthesized by Song *et al.* are coated with PVP and therefore hydrophilic. Pt@CoO nanoreactors are synthesized in *o*-dichlorobenzene requiring Pt nanoparticles bound by hydrophobic reagents. PVP is replaced on the shape-controlled Pt particles by ligand exchange. Pt nanoparticles are precipitated from ethylene glycol with acetone, followed by precipitation in hexane after which the Pt particles are redispersed in ethylene glycol containing 50 equivalents of hexadecanethiol (HDT). This solution is refluxed (190°C) overnight, followed by washing the HDT coated Pt particles with acetone and precipitation with hexane. Washing and precipitation after ligand exchange is repeated numerous times. Finally, the particles are dispersed in chloroform. Infrared spectroscopy of the exchanged particles demonstrates that > 80% of the PVP is exchanged for the long alkyl chain thiol.

Comparative Example 1: Catalytic activity of hollow nanocrystal without enclosed nanoparticle

Hollow cobalt oxide (CoO) nanoparticles were tested for ethylene hydrogenation to determine the catalytic activity of hollow CoO nanocrystals. The reactions were conducted in a plug flow reactor at ambient temperature and higher with ~75 mg of hollow CoO nanoparticles. No ethane formation was measured at ambient conditions for un-reduced and CoO hollow nanoparticles reduced at 100°C (373 K) for 1 h. Upon reduction at 473 K in 1 atm H<sub>2</sub>, CoO nanoparticles were active for ethylene hydrogenation at temperatures above room temperature. Catalyst activity was measured

from 295-353 K. With 75 mg of catalyst, no measurable activity below 0°C (273 K) was detectable by gas chromatography.

It is evident that the Pt containing CoO nanoreactor enables the catalytic hydrogenation to occur at much lower temperatures than with the hollow CoO nanoparticle. Samples containing platinum without pretreatment were active ethylene hydrogenation at temperatures as low as 208 K, while the CoO nanoparticles without pretreatment demonstrated no ethylene hydrogenation at room temperature. Only upon reduction at 473 K for 1 h. are the hollow CoO nanoparticles active for ethylene hydrogenation, see Yin, Y.; Rioux, R. M.; Erdonmez, C. K.; Hughes, S.; Somorjai, G. A.; Alivisatos, A. P. *Science* **304**, 711 (2004), the contents of which are incorporated by reference for all purposes. Comparative example 1 demonstrates that the Pt nanoparticles are responsible for catalyzing the hydrogenation of ethylene at low temperatures (208 K) and verifies that the polycrystalline CoO shell allows the diffusion of reactants and products into and out of the core, respectively. While not wishing to be bound by any particular theory or principle the most likely entry and exit points to the Pt core are grain boundaries.

Comparative Example 2: Comparison of activity of nanoreactors with prior art catalysts

A comparison of reactivity of Pt/CoO nanocatalysts with metal oxide supported Pt catalysts of the prior art for ethylene hydrogenation is shown in Table 1. The catalytic reactivity of the Pt/CoO nanocatalysts were compared with ethylene hydrogenation measurements made on a number of supported and unsupported Pt catalysts, see Grunes, J.; Zhu, J.; Anderson, E. A.; Somorjai, G. A. *J. Phys. Chem. B.* **106**, 11463 (2002), Zaera, F.; Somorjai, G. A. *J. Am. Chem. Soc.* **106**, 2288 (1984), Cortright, R. D.; Goddard, S.

A.; Rekoske, J. E.; Dumesic, J. A. *J. Catal.* **127**, 342 (1991), the contents of which are all incorporated by reference in their entirety for all purposes. All turnover frequencies were corrected to 10 Torr C<sub>2</sub>H<sub>4</sub>, 100 Torr H<sub>2</sub> and 298 K using reported activation energies and reaction orders for extrapolation. A comparison of the Pt nanoreactor materials with a number of Pt based catalysts (supported and unsupported) is compiled in Table 1.

TABLE 1

Catalyst	Corrected	Apparent Activation
	Turnover frequency <sup>a</sup> (s <sup>-1</sup> )	Energy, E <sub>a</sub> (kcal mol <sup>-1</sup> )
Pt nanoparticle array <sup>b</sup>	14.4	10.2
Pt(111) single crystal <sup>c</sup>	9.3	10.8
0.04% Pt/SiO <sub>2</sub> (cabosil) <sup>d</sup>	4.4	8.6
Pt wire <sup>d</sup>	2.7	8.6
14.2% Pt(5.4 nm)/CoO <sup>e</sup>	0.3	5.0
14.2% Pt(3.8 nm)/CoO	0.2	8.3

<sup>a</sup>Rates corrected to 10 Torr C<sub>2</sub>H<sub>4</sub>, 100 Torr H<sub>2</sub> and 298 K

<sup>b</sup>Grunes, J.; Zhu, J.; Anderson, E. A.; Somorjai, G. A. *J. Phys. Chem. B.* **106**, 11463 (2002)

<sup>c</sup>Zaera, F.; Somorjai, G. A. *J. Am. Chem. Soc.* **106**, 2288 (1984).

10 <sup>d</sup>Cortright, R. D.; Goddard, S. A.; Rekoske, J. E.; Dumesic, J. A. *J. Catal.* **127**, 342 (1991).

<sup>e</sup>Yin, Y.; Rioux, R. M.; Erdonmez, C. K.; Hughes, S.; Somorjai, G. A.; Alivisatos, A. P. *Science* **304**, 711 (2004).

Table 1 demonstrates that the turnover frequency for ethane production at room temperature is one order of magnitude lower than the catalyst (0.04% Pt/SiO<sub>2</sub>) with the most similar morphology, while the rate is approximately two orders of magnitude lower than the Pt nanoparticle array and single crystal. The above comparison assumes for the Pt/CoO nanoreactor catalyst that all Pt particles are accessible and their surfaces are

clean.

The terms and expressions which have been employed herein are used as terms of description and not of limitation, and there is no intention in the use of such terms and expressions of excluding equivalents of the features shown and described, or portions thereof, it being recognized that various modifications are possible within the scope of the invention claimed. Moreover, any one or more features of any embodiment of the invention may be combined with any one or more other features of any other embodiment of the invention, without departing from the scope of the invention.

All patents, patent applications, and publications mentioned above are herein incorporated by reference in their entirety for all purposes. None of the patents, patent applications, and publications mentioned above are admitted to be prior art.